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Fractal analysis of the effect of particle aggregation distribution on thermal conductivity of nanofluids (Revised)

Wei Wei, Jianchao Cai, Xiangyun Hu, Qi Han, Shuang Liu, Yingfang Zhou

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## Highlights

- A thermal conductivity model is derived based on fractal aggregation distribution.
- The relationship between aggregation shape and fractal dimension is analyzed.
- Predictions of the proposed model show good agreement with experimental data.

1           **Fractal analysis of the effect of particle aggregation**  
2           **distribution on thermal conductivity of nanofluids (Revised)**

3

4           Wei Wei<sup>1</sup>, Jianchao Cai<sup>1\*</sup>, Xiangyun Hu<sup>1</sup>, Qi Han<sup>1</sup>, Shuang Liu<sup>1</sup>, Yingfang Zhou<sup>2</sup>

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6           1. *Hubei Subsurface Multi-scale Imaging Key Laboratory, Institute of Geophysics and*  
7           *Geomatics, China University of Geosciences, Wuhan 430074, P.R. China*

8           2. *School of Engineering, University of Aberdeen, FN 264, King's College, Aberdeen,*  
9           *the UK, AB24 3UE*

10          \*Corresponding author.

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12          E-mail:

13          weiw2015@gmail.com (W. Wei)

14          caijc@cug.edu.cn (J. Cai)

15          xyhu@cug.edu.cn (X. Hu)

16          hanqi426@gmail.com (Q. Han)

17          lius@cug.edu.cn (S. Liu)

18          yingfang.zhou@abdn.ac.uk (Y. Zhou)

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20

21 **Abstract**

22 A theoretical effective thermal conductivity model is derived based on fractal  
23 distribution characteristics of nanoparticle aggregation. Considering two different  
24 mechanisms of heat conduction including particle aggregation and convection, the  
25 model is expressed as a function of the fractal dimension and concentration. In the  
26 model, the change of fractal dimension is related to the variation of aggregation shape.  
27 The theoretical computations of the developed model provide a good agreement with  
28 the experimental results, which may serve as an effective approach for quantitatively  
29 estimating the effective thermal conductivity of nanofluids.

30

31 **Highlights**

32 A thermal conductivity model is derived based on fractal aggregation distribution.  
33 The relationship between aggregation shape and fractal dimension is analyzed.  
34 Predictions of the proposed model show good agreement with experimental data.

35

36 **Keywords:** Thermal conductivity; Fractal; Aggregation distribution; Aggregation  
37 shape

38

39 **1. Introduction**

40 Quantitative estimate of the effective thermal conductivity has attracted substantial  
41 attentions since it is one of the most important parameters characterizing the heat  
42 transport properties of nanofluids [1-4]. Nanofluids are liquid suspensions that contain  
43 nanometer-size particles, with size much smaller than 100 nm, and their thermal  
44 conductivity is higher than that of their base liquids [5-8]. In recent years, a great  
45 amount of efforts has been exerted to study conductivity characteristic, and significant  
46 progress has been made towards the theoretical modeling [9-14] and laboratory  
47 experiments [15-19]. In 19th century, Maxwell [20] predicted that the thermal  
48 conductivity of mixtures increase by suspending some higher-conductivity substance  
49 such as solid particles. Since Maxwell model is only a first-order approximation, it  
50 applies only to mixtures with low particle volume fraction and small values of the ratio  
51 of thermal conductivity between particle and liquid [21]. Moreover, other traditional  
52 models for multiphase systems, such as Wiener approximation [22] and Bruggeman  
53 approach [23], fail to illuminate the abnormal enhancement of the effective thermal  
54 conductivity for low particle volume fraction in nanofluids.

55 Several researchers concluded that the major factors of heat conduction  
56 mechanisms in nanofluids including particle aggregation [24, 25], particle motion [26-  
57 28] and liquid-layering [9, 29]. Particularly, the fact that particle aggregation can  
58 enhance the effective thermal conductivity of nanofluids has been confirmed  
59 experimentally [30-32]. Wang et al. [33] claimed that particle clustering could  
60 prominently affect the enhancement of thermal conductivity of nanofluids. Hamilton  
61 and Crosser [34] presented a mixture model to explain heterogeneous two-component  
62 systems. In their model, the particle aggregation shape is invariable, which ignores the  
63 effect of aggregation shape on the effective thermal conductivity of nanofluids.

64 After fractal geometry was introduced by Mandelbrot [35], it became a powerful

65 tool for the analysis of physico-geometrical properties and processes, such as electricity  
 66 conductivity [36, 37], spontaneous capillary imbibition [38, 39], thermal conductivity  
 67 [40-44] and permeability [45-48]. Several researchers [33, 49-53] also apply fractal  
 68 geometry to study heat conduction of nanofluids. Wang et al. [33] established an  
 69 effective thermal conductivity model based on the effective medium approximation and  
 70 the fractal theory to describe nanoparticle cluster and radial distribution. Xu et al. [50]  
 71 applied fractal geometry to predict the thermal conductivity in terms of particles sizes  
 72 distribution and heat convection of nanofluids. Considering the effect of Brownian  
 73 motion of nanoparticles, Xiao et al. [52] presented a fractal model of thermal  
 74 conductivity which is expressed as a function of the average diameter of nanoparticles,  
 75 the nanoparticle concentration, the fractal dimension of nanoparticles and physical  
 76 properties of fluids.

77 To the best of our knowledge, there is no full relationship to depict the effective  
 78 thermal conductivity of nanofluids with fractal clustering distribution in terms of  
 79 particle aggregation and convection. In the present study, based on modified Hamilton  
 80 and Crosser model and Xu et al. model, an analytical model considering fractal  
 81 distribution characteristic of nanoparticle aggregation is derived to estimate the  
 82 effective thermal conductivity. The validity of the model was confirmed by comparison  
 83 with the experimental results.

84

## 85 **2. The fractal thermal conductivity model**

### 86 **2.1. Consideration of size effect of nanoparticles**

87 Hamilton and Crosser [34] used empirical shape factor  $F$  to consider the effect of  
 88 two heterogeneous phases and improved Maxwell equation [20] to calculate the  
 89 effective thermal conductivity of nanofluid  $k_s$  that is induced by stationary nanoparticles  
 90 in the liquids:

$$91 \quad k_s = k_f \frac{a + (F - 1) - (F - 1)(1 - \alpha)\phi}{a + (F - 1) + (1 - \alpha)\phi} \quad (1)$$

92 and

$$93 \quad F = \frac{3}{\psi} \quad (2)$$

94 where  $a = k_p / k_f$  ( $k_p$  is thermal conductivity of particle and  $k_f$  is thermal conductivity  
95 of fluid),  $\psi$  is defined as the ratio of the surface area  $A'_p$  of a sphere to the surface  
96 area  $A_p$  of the particle whose volume  $V_p$  equal to that of the sphere, therefore

$$97 \quad \psi = \frac{A'_p}{A_p} = \frac{6 V_p}{\lambda A_p} \quad (3)$$

98 where  $\lambda$  is aggregation size.

99 However,  $\lambda$  usually has different diameters due to aggregation in nanofluids and  
100 thus  $\psi$  is not a constant. According to Hamilton and Crosser,  $\psi = 1$  for spherical  
101 particle and  $\psi = 0.5$  for elliptic particle. If substituting  $\lambda$ ,  $V_p$  and  $A_p$  with  
102 average particle size  $\bar{\lambda}$ , average volume  $\bar{V}_p$  and average area  $\bar{A}_p$ , respectively, Eq.  
103 (3) can be deduced as

$$104 \quad \psi = \frac{A'_p}{A_p} = \frac{6 \bar{V}_p}{\bar{\lambda} \bar{A}_p} \quad (4)$$

105 It has been shown that the size distribution of aggregation in nanofluids follows  
106 the fractal power law [33, 49, 50]. Analogous to pores in fractal porous media, the  
107 fractal probability density function can be expressed as [50]

$$108 \quad f(x) = D \lambda_{\min}^D \lambda^{-(D+1)} d\lambda \quad (5)$$

109 The fractal dimension  $D$  is determined by [48]

$$110 \quad \xi = \phi^{\frac{1}{D_E - D}} \quad \text{or} \quad D = D_E - \frac{\ln \phi}{\ln \xi} \quad (6)$$

111 where  $D_E = 3$  for three-dimension space,  $\phi$  is the concentration of nanoparticles

112 and  $\xi = \lambda_{\min} / \lambda_{\max}$ , where  $\lambda_{\max}$  and  $\lambda_{\min}$  are the maximum and minimum diameters

113 of nanoparticle cluster, respectively. When the particle cluster has fractal characteristics,  
 114 its area and volume are  $\pi\lambda^2$  and  $\pi/6 \cdot \lambda^3$ , respectively, Eq. (4) can be expressed

$$115 \quad \psi = \frac{6 \int_{\lambda_{\min}}^{\lambda_{\max}} \frac{\pi}{6} \lambda^3 f(\lambda) d\lambda}{\bar{\lambda} \int_{\lambda_{\min}}^{\lambda_{\max}} \pi \lambda^2 f(\lambda) d\lambda} \quad (7)$$

116 Combining Eqs. (5), (6) and (7),  $\psi$  can be obtained as

$$117 \quad \psi = \frac{2-D}{3-D} \frac{\lambda_{\min}}{\bar{\lambda}} \frac{\phi^{-1}-1}{\phi^{\zeta_2}-1} \quad (8)$$

118 where  $\zeta_2 = (D-2)/(3-D)$  and  $\bar{\lambda}$  can be found from the statistical property of  
 119 fractal object [50], as

$$120 \quad \bar{\lambda} \approx \frac{D}{D-1} \lambda_{\min} \quad (9)$$

121 Inserting Eq. (9) into Eq. (8), the following equation can be obtained

$$122 \quad \psi = \frac{D-1}{D} \frac{2-D}{3-D} \frac{\phi^{-1}-1}{\phi^{\zeta_2}-1} \quad (10)$$

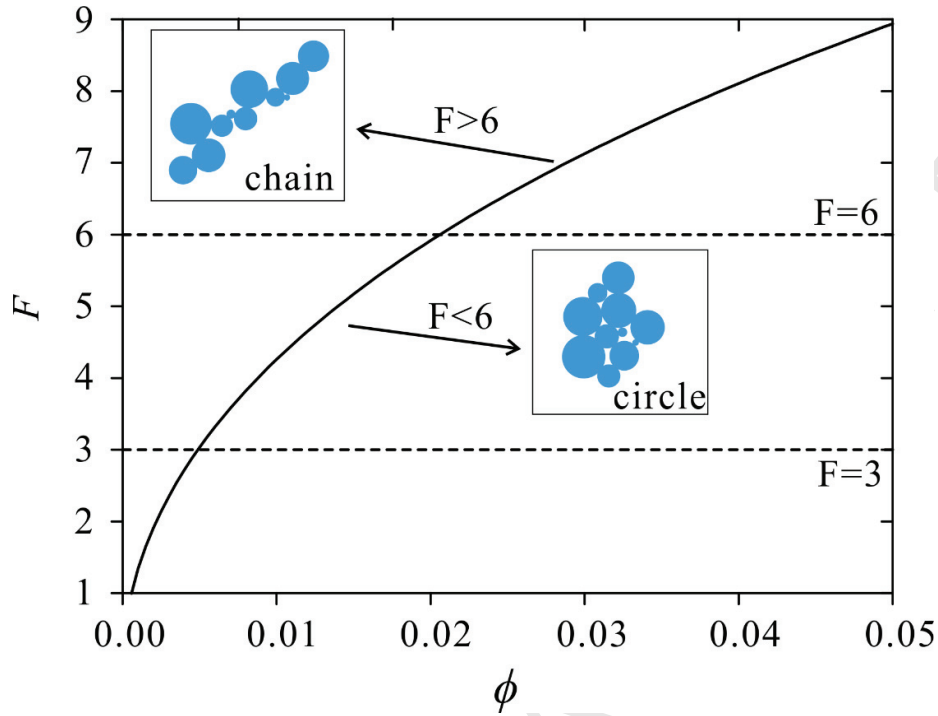
123 Therefore, inserting Eq. (10) into Eq. (2) yields

$$124 \quad F = 3 \frac{D}{D-1} \frac{3-D}{2-D} \frac{\phi^{\zeta_2}-1}{\phi^{-1}-1} \quad (11)$$

125 In Hamilton and Crosser's model,  $F$  is constant for same shape particles ( $F=6$  for  
 126 ellipse and  $F=3$  for sphere). However, it is observed that  $F$  is the function of fractal  
 127 dimension and concentration as expressed in Eq. (11), and  $F$  increase with the  
 128 increasing of concentration (see figure 1). As shown in figure 1, considering fractal  
 129 distribution of nanoparticle aggregation, the shape of aggregation gradually grow to  
 130 chain with the increasing concentration. When  $F < 6$ , most aggregation shapes are circles.  
 131 Eqs. (1) and (11) are the present fractal models that predict to effective thermal  
 132 conductivity of nanofluids relating with nanoparticles cluster.

133





134

135 Figure 1. Relationship between  $F$  and concentration  $\phi$  in Eq. (11). The dashed line for  
 136  $F=3$  and  $F=6$  [34] representing respectively sphere and ellipse for suspended  
 137 aggregation.

138

## 139 2.2. Consideration of convention effect of nanoparticles

140 Heat convection due to the Brownian motion of nanoparticles could enhance heat  
 141 transfer in nanofluids. While most convention models are based on an assumption that  
 142 suspended aggregation in nanofluids have uniform diameter. Xu et al. [50] theoretically  
 143 analyzed thermal conductivity  $k_c$  for heat convection by using the fractal geometry  
 144 for different sizes of nanoparticle cluster, which can be expressed as

$$145 \quad k_c = c \frac{k_f \cdot Nu \cdot d_f}{Pr} \frac{D(2-D)}{(1-D)^2} \frac{(\xi^{1-D} - 1)^2}{\xi^{2-D} - 1} \frac{1}{\bar{\lambda}} \quad (12)$$

146 where  $c$  is an empirical constant,  $Nu$  is the Nusselt number for liquid flowing around a  
 147 sphere,  $Pr$  is the Prandtl number for fluids and  $d_f$  is diameter of liquid molecule.  
 148 Combining Eq. (6) and Eq. (12), the following can be obtained

$$149 \quad k_c = c \frac{k_f \cdot Nu \cdot d_f}{Pr} \frac{(2-D)D}{(1-D)^2} \frac{(\phi^{\zeta_1} - 1)^2}{\phi^{\zeta_2} - 1} \frac{1}{\bar{\lambda}} \quad (13)$$

150 where  $\zeta_1 = (D-1)/(3-D)$ . The thermal conductivity for heat convection  $k_c$  can  
 151 express as a complex function of the Prandtl number  $Pr$ , the average diameter of  
 152 aggregation  $\bar{\lambda}$ , the diameter of molecule of fluids  $d_f$ , the concentration  $\phi$ , the Nusselt  
 153 number  $Nu$  and the fractal dimension  $D$ . Next section, the model will be simplified and  
 154 combine Eq. (1) to form a new effective thermal conductivity model with particle  
 155 aggregation and convection.

156

### 157 2.3. The present fractal thermal conductivity model

158 In this paper, we assume that the enhancement of thermal conductivity of  
 159 nanofluids may be caused by aggregation distribution in the liquids and Brownian  
 160 motion of clustering. Thus, the total dimensionless effective thermal conductivity  $k_e$   
 161 of nanofluids based on Eqs. (1), (11) and (12) can be written as

$$162 \quad k_e = \frac{k_s + k_c}{k_f} = \frac{a + (F-1) - (F-1)(1-\alpha)\phi}{a + (F-1) + (1-\alpha)\phi} + c \frac{Nu \cdot d_f}{Pr} \frac{(2-D)D}{(1-D)^2} \frac{(\phi^{\zeta_1} - 1)^2}{\phi^{\zeta_2} - 1} \frac{1}{\bar{\lambda}} \quad (14)$$

163 Xu et al. [50] found that the values of  $c$  is 85.0 both for the  $Al_2O_3$  nanoparticles  
 164 and for the  $CuO$  nanoparticles added in the deionized water, and  $c$  equates to 280.0 for  
 165 the ethylene glycol. The value of  $c$  is approximate to be  $\bar{\lambda}/d_f$ , then Eqs. (14) can be  
 166 deduced to

$$167 \quad k_e = \frac{a + (F-1) - (F-1)(1-\alpha)\phi}{a + (F-1) + (1-\alpha)\phi} + \frac{Nu (2-D)D}{Pr (1-D)^2} \frac{(\phi^{\zeta_1} - 1)^2}{\phi^{\zeta_2} - 1} \quad (15)$$

168 Eqs. (11) and (15) indicate that the total dimensionless effective thermal

169 conductivity  $k_e$  varies with the concentration and fractal dimension for nanoparticle  
170 aggregation. In the present model,  $Nu \approx 2$  and  $Pr \approx 6.0$  for water at room  
171 temperature [50]. Once the concentration  $\phi$  and the fractal dimension  $D$  are  
172 given/measured, the effective thermal conductivity can be calculated according to Eq.  
173 (15).

174

### 175 **3. Results and discussion**

176 To our knowledge, the fractal dimension has never been accurately measured to  
177 describe thermal conductivity for whole nanofluids. In the following, we therefore  
178 evaluate our proposed models (Eqs. (11) and (15)) by fitting experimental  
179 measurements, and discuss the relationship between fractal dimension and aggregation  
180 shape.

181 Wang et al. [33] measured the SiO<sub>2</sub>/ethanol nanofluids and obtained the fractal  
182 dimension equals to 1.57 for nanoparticles when  $\phi$  is about 6.5%. Their model predicted  
183 effective thermal conductivity of CuO/water nanofluids could reflect the variation of  
184 concentration  $\phi$  qualitatively. The result indicates that the local fractal characteristic  
185 represents whole fractal behavior of particles suspensions.

186 Figure 2 and figure 3 display the present model predictions with the available  
187 experimental data. Here the fractal dimension can be obtained by the nonlinear  
188 regression method based on Mean Squared Error (MSE) to estimate fitting results. The  
189 obtained fractal dimension is 1.572 from fitting to the nanofluids of CuO/water, is very  
190 close to the measured fractal dimension, 1.57, by Wang et al [33], which demonstrates  
191 the validity of the present model.

192 Table 1 show that good agreement is found between the predictions of proposed  
193 model and experiment results (lower MSE). Figure 2 also clearly indicates that the  
194 thermal conductivity of nanofluids increases with the increment of nanoparticles'  
195 concentration. It is notable that our proposed model fits better to  $k_e$  in the range of 1.1-

196 1.3 when  $0 < \phi < 0.05$ , so the model have not always fitted to lower  $k_e$ , such as  
 197  $\text{Al}_2\text{O}_3/\text{water}$  [54].

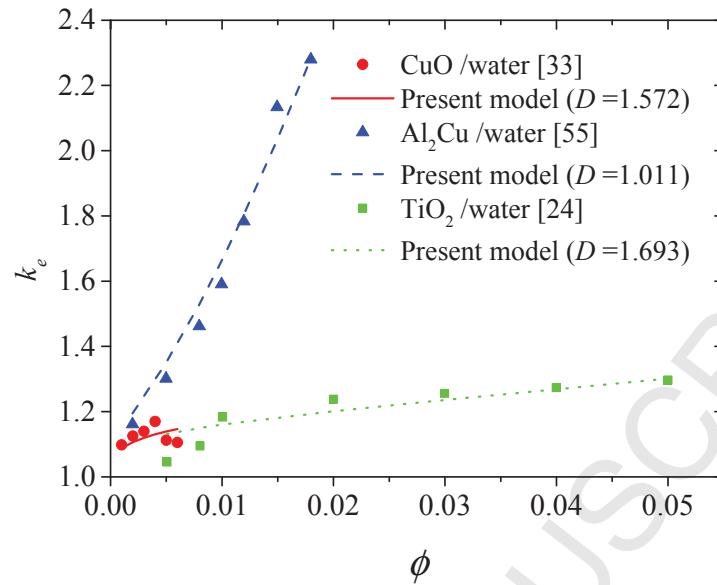
198 In Eq. (11),  $F$  is always less than 6 when fractal dimension is larger than a  
 199 particular value (the value is 1.2 in our model), such as  $D=1.693$  for  $\text{TiO}_2/\text{water}$  in  
 200 table 1. It indicates that the shape of aggregations are near circle, and the increased  
 201 speed of  $k_e$  becomes gradually slow with the increasing concentration. For nanofluids  
 202 of  $\text{Al}_2\text{Cu}/\text{water}$ , the fractal dimension  $D$  is approximately 1, which resulting to  $F > 6$  and  
 203  $k_e = 2.28$  in smaller concentration ( $\phi=0.018$ ). In this situation, aggregation shapes are  
 204 seem to be behaved as chain and thus play a major role in enhancing heat conduction  
 205 of nanofluids. Generally, smaller fractal dimension of nanofluids would produce more  
 206 aggregations of chain shape and enhance heat energy transfer. However, to demonstrate  
 207 the relationship between fractal dimension and  $F$ , more experiments and numerical  
 208 modeling are needed.

209

210 Table 1. Data for calculating the total dimensionless effective thermal conductivity

	$k_p$ (W/m/K)	$k_f$ (W/m/K)	$\bar{\lambda}$ (nm)	$D$	MSE (%)
CuO/water [33]	32.9	0.613	50.0	1.572	3.70
$\text{Al}_2\text{Cu}/\text{water}$ [55]	418.7	0.613	30.0	1.011	0.00
$\text{TiO}_2/\text{water}$ [24]	8.5	0.613	15.0	1.693	1.92

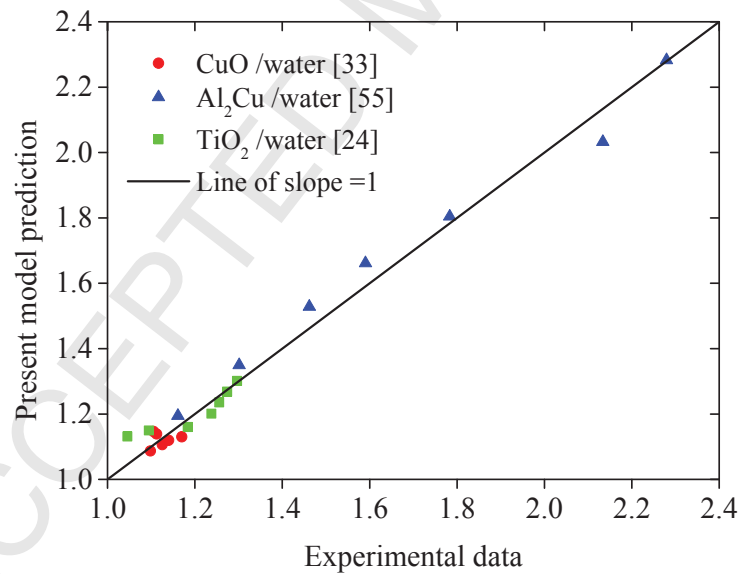
211



212

213 Fig. 2. Comparison between the total dimensionless effective thermal conductivity  $k_e$ 214 from fractal model and experimental data in different concentration  $\phi$ .

215



216

217 Fig. 3. A comparison of the experimental data with the present model predictions.

218

219 **4. Conclusions**

220 In this paper, an analytical expression to calculate the thermal conductivity in

221 nanofluids with different space distribution of aggregation is derived base on fractal  
222 geometry. The model, which takes into account  $F$  in Hamilton and Crosser, is a function  
223 of fractal dimension of nanoparticle aggregation and concentration in nanofluids. The  
224 effective thermal conductivity calculated based on the developed model provides a  
225 good agreement with the experimental results, which validates the validity of the model.  
226 The concentration-dependent total dimensionless effective thermal conductivity of  
227 three kinds of nanofluids were analyzed. Results show that the fractal dimension may  
228 influence the variation of aggregation shape, and more experiment analyses are needed  
229 to further quantitatively estimate the influence.

230 The present study only focus on the effect of particle aggregation and convention  
231 for heat conduction mechanism. In the future, more aggregation patterns of nanofluids  
232 will be tested and the model will be improved to consider the effect of liquid-layering.

233

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316 **Figure captions**

317 Fig. 1. Relationship between  $F$  and concentration  $\phi$  in Eq. (11). The dashed line for  $F=3$   
318 and  $F=6$  [34] representing respectively sphere and ellipse for suspended  
319 aggregation.

320 Fig. 2. Comparison between the total dimensionless effective thermal conductivity  $k_e$   
321 from fractal model and experimental data in different concentration  $\phi$ .

322 Fig. 3. A comparison of the experimental data with the present model predictions.

323 **Tables**

324 Table 1. Data for calculating the total dimensionless effective thermal conductivity

	$k_p$ (W/m/K)	$k_f$ (W/m/K)	$\bar{\lambda}$ (nm)	$D$	MSE (%)
CuO/water [33]	32.9	0.613	50.0	1.572	3.70
Al <sub>2</sub> Cu/water [55]	418.7	0.613	30.0	1.011	0.00
TiO <sub>2</sub> /water [24]	8.5	0.613	15.0	1.693	1.92

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